First Hybrid Turbulence Modeling for Turbine Blade Cooling

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Introduction

AS turbines require proper cooling mechanisms to protect the airfoils from thermal stresses generated by exposure to hot combustion gases. The problem becomes aggravated by the growing trend to use higher turbine inlet temperatures to generate more power. Thus, film cooling is used as a cooling mechanism, and it works in the form of row of holes located in the spanwise direction, through which cold jets are issued into the hot crossflow. The penetration of cold jets into the main flow creates a complex flowfield. Systematic investigation of such flowfield started in late 1950s. Figure 1 shows the schematic of a single round jet injected in the crossflow at an angle $\alpha = 35$ deg. The figure also describes the boundary conditions applied at different faces. Even though use of symmetry boundary condition at the hole centerline would reduce the computational time by half, its use is avoided as it prevents the possibility of capturing the unsteady asymmetric vortical flow patterns. This geometry is well accepted by the gas-turbine community and has been extensively studied1 for cooling performance for a wide range of blowing ratios, $M = \rho_j V_j/\rho_{\rm fs} V_{\rm fs}$, where ρ and V are density and normal velocity, respectively, for jet *j* and freestream fs.

Goldstein² correlated film cooling effectiveness $\eta = (T_{\rm fs} - T)/(T_{\rm fs} - T_j)$ with the parameter x/Mb, where x is the downstream distance; M is the blowing ratio; b is the slot width; and $T_{\rm fs}$, T, and T_j are the temperatures of crossflow, blade, and jet, respectively. Sinha et al. carried out experimental work to study the relationship between the fluid-thermal parameters of jet and film cooling effectiveness using a row of inclined holes.

The mixing of a jet in a cross stream is a fully three-dimensional phenomenon.³ Amer et al.⁴ pointed out that the flow predictions are greatly affected by the selection of the turbulence model. Roy⁵ documented the cooling performance of 12 different arrangements of holes with a combination of blowing ratio M, distance between the holes L, and jet angle α using a upwind-biased finite volume code and standard $k-\omega$ turbulence closure model. Garg and Rigby⁶ resolved the plenum and hole pipes for a three-row showerhead film cooling arrangement with Wilcox's $k-\omega$ turbulence model. Heidmann et al.⁷ used Reynolds-averaged Navier–Stokes (RANS) to compute the heat transfer for a realistic turbine vane with 12 rows of film cooling holes with shaped holes and plena resolved. Though these studies provide good details of the flow, the anisotropic dynamic nature of the spanwise vortices that affect the film cooling process are more complex than that can be captured by the mixing models used in aforementioned papers. Acharya⁸ compared the re-

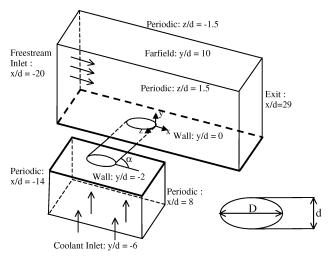


Fig. 1 Schematic of the film cooling flow. Actual geometry definition and boundary conditions are based on Sinha et al.¹

sults of $k-\varepsilon$ and Reynolds-stress-transport turbulence models with the data of direct numerical simulation (DNS) and large-eddy simulation (LES) for a film cooling problem and concluded that as compared to DNS and LES two-equation RANS models generally underpredict the lateral spreading of the jet and overpredict the penetration because of an assumption of isotropic eddy viscosity. Though DNS and LES can capture minor flow details, these methods are computationally limited for high-Reynolds-number flows. For $Re = 4.7 \times 10^3$, the LES solution on $122 \times 52 \times 32$ node mesh took 1-2 days in Digital Alpha 500 workstation. As a viable alternative, this Note presents the first detached-eddy-simulation (DES)-based hybrid modeling of film cooling flow for the three-dimensional geometry in Fig. 1. The result is also compared with the centerline and spanwise effectiveness obtained by the experiment of Sinha et al.

Hybrid Turbulence Model

The two competing factors important for any turbulence model are accuracy and efficiency (i.e., computational cost). Proposed by Spalart et al., DES is a hybrid model that combines the efficiency of RANS and the accuracy of LES length scales to work under a single framework. DES works by applying a variable length scale that varies as a function of the distance to the nearest wall d_w in the attached boundary layer and conforms with subgrid scale in the rest of the flow including separated regions and near wake. Two different DES models 10,11 are currently available in the numerical code 12 used in the present simulation: 1) (Spalart–Allmaras) (S–A) based DES model and 2) Menter's shear-stress transport based DES model. A Spalart–Allmaras-based DES model 13 is used in the present study. S–A is a one-equation RANS model. Detailed information about S–A one-equation model, which is used in the presented DES simulation, is given by Squires et al. 11

A Spalart–Allmaras-based DES model has been developed in such a way that the model works as a S–A RANS model near the wall surfaces and acts as a subgrid LES model away from the wall. In an S–A-based DES formulation, distance to the nearest wall d_w is replaced by \tilde{d} , where \tilde{d} is defined as

$$\tilde{d} = \min(d_w, C_{\text{DFS}}\Delta) \tag{1}$$

where $C_{\rm DES}$ is a model constant, and for the S–A based DES model $C_{\rm DES} = 0.65$ and Δ is the largest distance between the cell center under consideration and the cell center of the neighbors. The model works as a standard S–A turbulence model inside the numerically predicted boundary layer. In the regions far from the wall, where $d_w > C_{\rm DES} \Delta$, the length scale becomes grid dependent, and the model performs as a subgrid-scale version of the S–A model for eddy viscosity. When production and destruction terms balance each other, this model reduces to an algebraic mixing-length Smagorinski-like subgrid model. Recently, Kapadia et al. ¹⁴ have

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successfully implemented DES for external flow analysis over a ground vehicle.

Grid Information and Computational Approach

The present study implements Cobalt, 12 a parallel, implicit, unstructured finite volume based flow solver that uses second-orderaccurate spatial and temporal Godunov schemes. 15 A multiblock computational grid was initially developed using the GridPro Multiblock grid generator with 15 blocks and approximately 2,600,000 computational cells. Gridgen14.03 is used to convert this grid into a Cobalt-compatible unstructured grid. The final grid used in the solution contains a single block and 2,109,440 cells, which is approximately 10 times the size of Acharya's mesh.8 The Reynolds number based on the diameter and inlet conditions at the hole was 1.97×10^4 . Viscous clustering was employed at all solid walls with a y⁺ value less than 1.0 at all locations. Stretching ratios less than 1.2 were used normal to the viscous walls. Iteration convergence was considered achieved when all residuals reduce by four orders of magnitude. The size of the time step is a function of Courant-Friedrichs-Lewy, which increases from 10³ to 10⁶ during the initial 130 time steps and remains constant for the remaining time steps, yielding the maximum time-step size of 6.17×10^{-4} s. The present case is run on the cluster of 64 parallel processors on Blue Horizon supercomputer at San Diego Supercomputing Center (SDSC). The aggregate CPU time requirement for the entire DES solution is 37.46 s/iteration and that for one cell is 17.76 MS/iteration. Total CPU requirement for the solution to complete 6000 time steps (real time 3.7 s) is approximately 4000 h. Extrapolating, it is easy to estimate that for a coarser mesh⁸ DES solution will take less than 16 h. As size of the time step is not very small in the present case, simulation was run using two Newton subiterations to reduce linearization errors in the Jacobian. This increased the computational time by three times normal iteration (without Newton subiteration, which is common for a steady-state solution).

Results and Discussion

Figure 1 describes schematic control volume, in which hot air at 300 K passes over a flat surface and cool air at 150 K is issued at an angle $\alpha = 35$ deg. The intersection of the injection pipe with the wind tunnel forms an ellipse with the minor and the major axes of d = 2.54 mm and $D = d/(\sin \alpha)$, respectively. The presented numerical simulation uses blowing ratio of 1, density ratio of 2, and velocity ratio of 0.5. Fixed mass flow rate and stagnation temperature inlet boundary conditions are employed for the plenum and freestream. A fixed static pressure boundary condition is applied at the exit. Adiabatic no-slip conditions are applied at all solid walls, including the inner surface of the film hole and the plenum. A maximum Mach number not exceeding 0.3 was achieved in the flowfield while maintaining the desired Reynolds number by scaling the experimental geometry¹ down by a factor of 5. Figures 2–6 described in this section correspond to the time-averaged DES solution after 3.7 s, when solution reaches a quasi-stationary state.

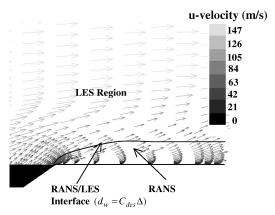


Fig. 2 DES/RANS interface and velocity vectors colored by u velocity at hole centerline (z=0).

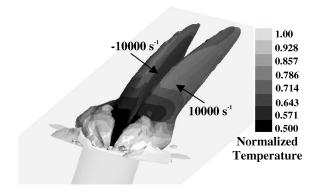


Fig. 3 Two isosurfaces of x vorticity (-10 K and 10 K) colored by the temperature.

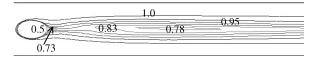


Fig. 4 Temperature contours normalized by the freestream temperature.

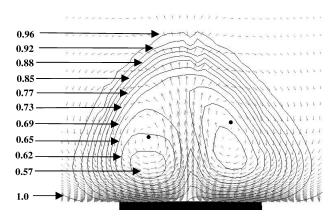
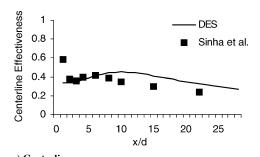


Fig. 5 Velocity vectors with superimposed normalized temperature contours at x/d = 3.5 for time-averaged DES solution.



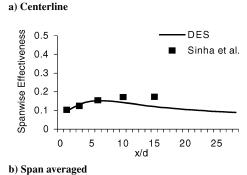


Fig. 6 Comparison between experimental and numerical effectiveness.

Figure 2 shows velocity vectors highlighted by the magnitude of streamwise velocity at the hole centerline (z=0). It also shows the interface between the RANS and LES region, where $d_w=C_{\rm des}\Delta$. It is evident from the figure that the treatment of the initial penetration of jet into freestream is carried out by pure LES technique. This is because of the fine spanwise spacing at the hole exit that switches the code to LES mode.

Figure 3 shows two isosurfaces of x vorticity colored by temperature. The values of the x vorticity for the left and right isosurfaces are $-10,000 \, \mathrm{s^{-1}}$ and $+10,000 \, \mathrm{s^{-1}}$, respectively. Light and dark shades of grayscales represent 300 and 150 K, respectively. The injection pipe is shown as reference. It is evident that maximum recirculation is present at the location of initial interaction between the jet and crossflow. The recirculation near the wake region follows a pair of counter-rotating vortices. A sharp temperature gradient is present near the trailing edge of the hole, which becomes more diffused as the flow progresses downstream.

The normalized wall temperature distribution in Fig. 4 indicates that the minimum temperature (0.5) exists at the hole. Downstream maximum cooling takes place in a small area just beyond (less than 1d) the trailing edge of the hole where the normalized wall temperature is 0.73. In the streamwise direction beginning at approximately 6d, the normalized temperature reduces to 0.78 and remains cool for nearly 7d.

Film cooling is a strongly coupled fluid-thermal process. Figure 5 plots the effect of flow structures on normalized fluid temperature on a vertical plane at x = 3.5d. The presence of asymmetry is present in the unsteady solution for both velocity vectors and temperature profile. Time-averaged data show prominent features of elongated kidney-shaped bound vortices followed by similar temperature profiles.

Comparison between experimental¹ and numerical (time-averaged DES) values of the centerline and the span-averaged effectiveness is done in Figs. 6a and 6b, respectively. The sharp difference between the experimental¹ and DES time-averaged results for centerline effectiveness at x = 1d stems from the fact that although numerical prediction of maximum cooling occurs near the trailing edge of the hole (similar to the experimental data), its streamwise distribution is very narrow, less than 1d (Fig. 4). The experimental and numerical effectiveness follow similar trend between x = 1d-6d. Beyond 6d, numerical centerline effectiveness shows higher value than the experimental data, whereas numerical span-averaged effectiveness is lower in that region. Figure 4 clearly shows that there is very little diffusion in the spanwise direction for DES results, which is responsible for the small values of span-averaged effectiveness.

Conclusions

The first detached eddy simulation of film cooling has been presented for a widely published plate-pipe configuration. The blowing ratio was unity and density ratio was two. Results indicate that the mixing processes downstream of the hole are highly anisotropic. DES solution shows its ability to depict the dynamic nature of the flow and capture the asymmetry present in temperature and velocity distributions. Further, comparison between experimental and DES time-averaged effectiveness is satisfactory. Numerical values of centerline and span-averaged effectiveness differ from those of experimental values at downstream locations. Smaller values of numerically predicted spanwise effectiveness than the experimental data might be caused by the improper turbulence model in the spanwise spreading of the jet. This needs to be investigated in the near future.

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Accelerated Solution of the Radiation-Transfer Equation with Strong Scattering

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Introduction

THIS Note explains why a method used to accelerate the solution of the radiation-transfer equation (RTE) breaks down, for fine grids, when applied to a purely scattering medium. The explanation is substantiated by showing that a simple strategy can eliminate the problem.

Radiation transfer in a participating medium can be solved in many ways, including the discrete ordinates¹ and the finite volume methods.² In these methods the intensities are calculated at discrete nodes in space and for specified directions (or within specified solid angles). For problems involving scattering, the intensity in one direction is usually dependent on the intensities in all other directions. To avoid solving the equations for all directions simultaneously, the

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